

High Vacuum System Engineering Calculations
2.75" Conflat High Vacuum System
Design Iteration #2
Transitional Flow with Deuterium at 20C

CONDUCTANCE CALCULATIONS – TRANSITIONAL FLOW
(For Use with Deuterium Injected Fusor Systems @ 10⁻² Torr)

1.) Diffusion Pump

→ Max Pumping Speed of Diffusion Pump @ 10⁻² torr

→ $S_{diff(k)} = 100 \text{ l/sec}$

2.) Transitional Flow Conductance for Diffusion Pump to 2.75" Conflat Adapter Plate

→ Conductance of Pipes in Transitional Flow

$$C_k = C_m \left(0.0736 \frac{D}{\lambda} + \frac{1+1.25D/\lambda}{1+1.55D/\lambda} \right)$$

C_k = transitional flow conductance

C_m = conductance for molecular flow = $C_{adapter} = 249.147 \text{ l/s}$

D = diameter (cm) = 3.556

λ = mean free path at average pressure ($P=10^{-2}$ torr) (cm) = 0.5

$C_k = 335.350 \text{ l/sec}$

→ $C_{k(adapter)} = 335.350 \text{ l/sec}$

3.) Transitional Flow Conductance for 2.75" Conflat Inline Poppet Valve

→ Conductance of Pipes in Transitional Flow

$$C_k = C_m \left(0.0736 \frac{D}{\lambda} + \frac{1+1.25D/\lambda}{1+1.55D/\lambda} \right)$$

C_k = transitional flow conductance

C_m = conductance for molecular flow = $C_{poppet_valve} = 91.932 \text{ l/s}$

D = diameter (cm) = 3.556

λ = mean free path at average pressure ($P=10^{-2}$ torr) (cm) = 0.5

$C_k = 123.740 \text{ l/sec}$

→ $C_{k(poppet_valve)} = 123.740 \text{ l/sec}$

4.) Transitional Flow Conductance for 2.75" Conflat Butterfly Valve

→ Conductance of Pipes in Transitional Flow

$$C_k = C_m \left(0.0736 \frac{D}{\lambda} + \frac{1+1.25D/\lambda}{1+1.55D/\lambda} \right)$$

C_k = transitional flow conductance

C_m = conductance for molecular flow = $C_{butterfly_valve} = 163.939 \text{ l/s}$

D = diameter (cm) = 3.556

λ = mean free path at average pressure ($P=10^{-2}$ torr) (cm) = 0.5

$C_k = 220.661 \text{ l/sec}$

$$\rightarrow C_{k(\text{butterfly_valve})} = 220.661 \text{ l/sec}$$

5.) Transitional Flow Conductance for 2.75" Conflat 4-Way Cross

→ Conductance of Pipes in Transitional Flow

$$C_k = C_m \left(0.0736 \frac{D}{\lambda} + \frac{1+1.25D/\lambda}{1+1.55D/\lambda} \right)$$

C_k = transitional flow conductance

C_m = conductance for molecular flow = $C_{\text{cross}} = 108.857 \text{ l/s}$

D = diameter (cm) = 3.556

λ = mean free path at average pressure ($P=10^{-2}$ torr) (cm) = 0.5

$$C_k = 146.521 \text{ l/sec}$$

$$\rightarrow C_{k(\text{cross})} = 146.521 \text{ l/sec}$$

6.) Total System Conductance

→ Conductance of Pipeline

$$\frac{1}{C_{k(\text{pipeline})}} = \frac{1}{C_{k(\text{adapter})}} + \frac{1}{C_{k(\text{poppet_valve})}} + \frac{1}{C_{k(\text{butterfly_valve})}} + \frac{1}{C_{k(\text{cross})}}$$

$$\frac{1}{C_{k(\text{pipeline})}} = \frac{1}{335.350} + \frac{1}{123.740} + \frac{1}{220.661} + \frac{1}{146.521}$$

$$C_{k(\text{pipeline})} = 11.760 \text{ l/sec}$$

$$\rightarrow C_{k(\text{pipeline})} = 44.603 \text{ l/sec}$$

→ Effective Pumping Speed of the System

$$\frac{1}{S_{e(k)}} = \frac{1}{C_{k(\text{pipeline})}} + \frac{1}{S_{\text{diff}(k)}}$$

$$S_{e(k)} = \frac{C_{k(\text{pipeline})} \times S_{\text{diff}(k)}}{C_{k(\text{pipeline})} + S_{\text{diff}(k)}}$$

$$C_{k(\text{pipeline})} = 8.737 \text{ l/s}$$

$$S_{\text{diff}(k)} = 100 \text{ l/s}$$

$$S_{e(k)} = 9.103 \text{ l/s}$$

$$\rightarrow S_{e(k)} = 30.845 \text{ l/sec}$$