

Foreline Parameters and Roughing Pumpdown Times
 From Atmosphere to Rough Vacuum
 2.75" Conflat Multipurpose High Vacuum Chamber V4

1.) Foreline Parameters

a.) Determination of Roughing Flow Regime

for: $D\bar{p} > 5 \times 10^{-1} \text{ Torr} \cdot \text{cm} \rightarrow \text{flow is purely viscous}$

for: $D\bar{p} < 1.5 \times 10^{-2} \text{ Torr} \cdot \text{cm} \rightarrow \text{flow is purely molecular}$

for: $1.5 \times 10^{-2} \text{ Torr} \cdot \text{cm} < D\bar{p} < 5 \times 10^{-1} \text{ Torr} \cdot \text{cm} \rightarrow \text{flow is transitional}$

$D = \text{diameter of roughing line (cm)} = 2.210 \text{ cm}$

$\bar{p} = \text{mean gas pressure (torr)} = \frac{1}{2}(P_1 + P_2) = \frac{1}{2}(760 + 0.02) = 380.010 \text{ Torr}$

$D\bar{p} = 839.822 \text{ Torr} \cdot \text{cm} \rightarrow \text{flow is purely viscous}$

b.) Conductance for Viscous Flow

$$C_\eta = \frac{\pi D^4}{128 L \eta} \bar{p} \text{ L/s}$$

$D = \text{diameter of roughing line (cm)} = 2.210 \text{ cm}$

$L = \text{length of roughing line (cm)} = 39.767 \text{ cm}$

$\eta = \text{viscosity of gas}$

$\bar{p} = \text{mean gas pressure (torr)} = \frac{1}{2}(P_1 + P_2) = \frac{1}{2}(760 + 0.02) = 380.010 \text{ Torr}$

for: AIR @ 20C,

$$C_\eta = \frac{182 D^4 \bar{p}}{L} \text{ L/s}$$

$C_\eta = 41487.062 \text{ L/s}$

c.) Effective Pumping Speed of Forepump in Viscous Flow

$$S_{e(\eta)} = \frac{C_\eta \times S_{\text{forepump}}}{C_\eta + S_{\text{forepump}}}$$

$S_{\text{forepump}} = \text{speed of forepump (L/s)} = 6 \text{ cfm} = 2.830 \text{ L/s}$

$C_\eta = \text{conductance for viscous flow of foreline (L/s)} = 41487.062 \text{ L/s}$

$S_{e(\eta)} \approx 2.83 \text{ L/s} \rightarrow \text{conductance of foreline is negligible to pumping speed}$

2.) Pumpdown Time for Rotary Pumps in the Roughing Region

for: pressures of 760 Torr – 10^{-2} Torr, $Q_{\text{outgassing}}$ is negligible

for: good design of forelines, effective speed (S_e) = speed at pump throat (S_b)

$$\tau = -\frac{V}{S_b} \int_{P_1}^{P_2} \frac{dp}{P - P'_u} \rightarrow$$

$$\tau = \frac{V}{S_b} \ln \left[\frac{P_1 - P'_u}{P_2 - P'_u} \right]$$

$V = \text{volume (liters)}$

$S_b = \text{speed at pump throat (L/s)} = 2.83 \text{ L/s}$

$P_1 = \text{starting pressure (Torr)} = 760 \text{ Torr}$

$P_2 = \text{ending pressure (Torr)} = 0.020 \text{ Torr}$

$P'_u = \text{ultimate pressure attainable by forepump (Torr)} = 0.015 \text{ Torr}$

for: V is volume of entire system from roughing pump to the chamber,

$$V_{total} = V_{foreline} + V_{diffusion_pump} + V_{pipeline} + V_{chamber}$$

$$V_{foreline} = V_{trap} + V_{bellows} + V_{KF25_tee} + V_{valve}$$

$$V_{foreline} = 152.545 \text{ cm}^3$$

$$V_{foreline} = 0.153 \text{ L}$$

$$V_{diffusion_pump} = V_{roughing_inlet} + V_{body}$$

$$V_{diffusion_pump} = 4388.187 \text{ cm}^3$$

$$V_{diffusion_pump} = 4.388 \text{ L}$$

$$V_{pipeline} = V_{baffle_adapter} + V_{baffle} + V_{plate_adapter} + V_{cross} + V_{valve}$$

$$V_{pipeline} = 613.237 \text{ cm}^3$$

$$V_{pipeline} = 0.613 \text{ L}$$

$$V_{chamber} = V_{chamber}$$

$$V_{chamber} = 310.160 \text{ cm}^3$$

$$V_{chamber} = 0.310 \text{ L}$$

$$V_{total} = 5.464 \text{ L}$$

$$\tau = \frac{V}{S_b} \ln \left[\frac{P_1 - P'_u}{P_2 - P'_u} \right]$$

$$V = \text{volume (liters)} = 5.464 \text{ L}$$

$S_b = \text{speed at pump throat (L/s)} = 2.830 \text{ L/s}$

$P_1 = \text{starting pressure (Torr)} = 760 \text{ Torr}$

$P_2 = \text{ending pressure (Torr)} = 0.020 \text{ Torr}$

$P'_u = \text{ultimate pressure attainable by forepump (Torr)} = 0.015 \text{ Torr}$

$$\tau = 23.037 \text{ seconds}$$