

APPLIED ION SYSTEMS

High Vacuum Engineering Calculations

Small-Scale Multipurpose High Vacuum System V5 Design
System Conductance and Effective Speed - Molecular Flow with Water Vapor at 20C

1.) Diffusion Pump

→ Max Pumping Speed of Diffusion Pump (Derived Estimate for Water Vapor)

→ **$S_{diff} = 624 \text{ l/sec}$**

2.) Diffusion Pump to Water Cooled Baffle Adapter (@ 20C)

→ Conductance of a Tube

$$C_m = 3.8 \left(\frac{T}{M} \right)^{\frac{1}{2}} \frac{D^3}{L}$$

C_m = conductance (l/sec)

T = temperature (K) = 293.15

M = molecular mass = 18.020 (average AMU of water vapor)

D = diameter (cm) = 12.70

L = length (cm) = 2.54

$C_m = 12360.288 \text{ l/sec}$

→ Conductance of a Short Tube

$$C_{short} = C_m \left(1 + \frac{4D}{3L} \right)^{-1}$$

C_{short} = conductance of short tube (l/sec)

C_m = conductance of a long tube (l/sec) = 12360.288

D = diameter (cm) = 12.70

L = length (cm) = 2.54

$C_{short} = 1612.212 \text{ l/sec}$

→ for $L/D < 5$, above equation is valid for short pipes, with error

$$L/D = 0.200$$

~+12% error max:

$$C_{shortFinal} = C_{short} \times 0.88$$

$C_{shortFinal} = 1418.746 \text{ l/sec}$

→ **$C_{baffle_adapter} = 1418.746 \text{ l/sec}$**

3.) Water Cooled Baffle (@ 20C)

→ Conductance of a Tube

$$C_m = 3.8 \left(\frac{T}{M} \right)^{\frac{1}{2}} \frac{D^3}{L}$$

C_m = conductance (l/sec)

T = temperature (K) = 293.15

M = molecular mass = 18.020 (average AMU of water vapor)

D = diameter (cm) = 18.415

L = length (cm) = 5.08

$$C_m = 18840.942 \text{ l/sec}$$

→ Conductance of a Short Tube

$$C_{short} = C_m \left(1 + \frac{4D}{3L}\right)^{-1}$$

C_{short} = conductance of short tube (l/sec)

C_m = conductance of a long tube (l/sec) = 18840.942

D = diameter (cm) = 18.415

L = length (cm) = 5.08

$$C_{short} = 3229.876 \text{ l/sec}$$

→ for $L/D < 5$, above equation is valid for short pipes, with error

$$L/D = 0.276$$

~+12% error max:

$$C_{shortFinal} = C_{short} \times 0.88$$

$$C_{shortFinal} = 2842.291 \text{ l/sec}$$

→ Correction for Baffle Fins

$$C_{shortFinal} = C_{short} \times 0.50$$

$$C_{shortFinal} = 1421.145 \text{ l/sec}$$

→ $C_{baffle} = 1421.145 \text{ l/sec}$

4.) Diffusion Pump to 6" Conflat Adapter Plate

→ Conductance of a Tube

$$C_m = 3.8 \left(\frac{T}{M}\right)^{\frac{1}{2}} \frac{D^3}{L}$$

C_m = conductance (l/sec)

T = temperature (K) = 293.15

M = molecular mass = 18.020 (average AMU of water vapor)

D = diameter (cm) = 10.16

L = length (cm) = 2.54

$$C_m = 6328.468 \text{ l/sec}$$

→ Conductance of a Short Tube

$$C_{short} = C_m \left(1 + \frac{4D}{3L}\right)^{-1}$$

C_{short} = conductance of short tube (l/sec)

C_m = conductance of a long tube (l/sec) = 6328.468

D = diameter (cm) = 10.16

L = length (cm) = 2.54

$$C_{short} = 999.232 \text{ l/sec}$$

→ for $L/D < 5$, above equation is valid for short pipes, with error

$$L/D = 0.250$$

~+12% error max:

$$C_{shortFinal} = C_{short} \times 0.88$$

$$C_{shortFinal} = 879.324 \text{ l/sec}$$

→ $C_{plate\ adapter} = 879.324 \text{ l/sec}$

5.) 6" to 2.75" Conflat Zero Clearance Reducer

→ Conductance of a Tube

$$C_m = 3.8 \left(\frac{T}{M} \right)^{\frac{1}{2}} \frac{D^3}{L}$$

C_m = conductance (l/sec)

T = temperature (K) = 293.15

M = molecular mass = 18.020 (average AMU of water vapor)

D = diameter (cm) = 3.988

L = length (cm) = 1.918

$$C_m = 506.837 \text{ l/sec}$$

→ Conductance of a Short Tube

$$C_{short} = C_m \left(1 + \frac{4D}{3L} \right)^{-1}$$

C_{short} = conductance of short tube (l/sec)

C_m = conductance of a long tube (l/sec) = 506.837

D = diameter (cm) = 3.988

L = length (cm) = 1.918

$$C_{short} = 134.356 \text{ l/sec}$$

→ for $L/D < 5$, above equation is valid for short pipes, with error

$$L/D = 0.481$$

~+12% error max:

$$C_{shortFinal} = C_{short} \times 0.88$$

$$C_{shortFinal} = 118.234 \text{ l/sec}$$

→ **$C_{reducer} = 118.234 \text{ l/sec}$**

6.) 2.75" Conflat 4-Way Cross

→ Conductance of a Tube

$$C_m = 3.8 \left(\frac{T}{M} \right)^{\frac{1}{2}} \frac{D^3}{L}$$

C_m = conductance (l/sec)

T = temperature (K) = 293.15

M = molecular mass = 18.020 (average AMU of water vapor)

D = diameter (cm) = 3.556

L = length (cm) = 12.492

$$C_m = 55.170 \text{ l/sec}$$

→ Conductance of a Short Tube

$$C_{short} = C_m \left(1 + \frac{4D}{3L} \right)^{-1}$$

C_{short} = conductance of short tube (l/sec)

C_m = conductance of a long tube (l/sec) = 43.511

D = diameter (cm) = 3.556

L = length (cm) = 12.492

$$C_{short} = 39.991 \text{ l/sec}$$

→ for $L/D < 5$, above equation is valid for short pipes, with error

$$L/D = 3.5$$

~+9% error max:

$$C_{shortFinal} = C_{short} \times 0.91$$

$$C_{shortFinal} = 36.392 \text{ l/sec}$$

$$\rightarrow C_{cross} = 36.392 \text{ l/sec}$$

7.) 2.75" Conflat Gate Valve

→ Conductance of a Tube

$$C_m = 3.8 \left(\frac{T}{M} \right)^{\frac{1}{2}} \frac{D^3}{L}$$

C_m = conductance (l/sec)

T = temperature (K) = 293.15

M = molecular mass = 18.020 (average AMU of water vapor)

D = diameter (cm) = 3.810

L = length (cm) = 5.050

$$C_m = 166.864 \text{ l/sec}$$

→ Conductance of a Short Tube

$$C_{short} = C_m \left(1 + \frac{4D}{3L} \right)^{-1}$$

C_{short} = conductance of short tube (l/sec)

C_m = conductance of a long tube (l/sec) = 166.864

D = diameter (cm) = 3.556

L = length (cm) = 2.54

$$C_{short} = 83.432 \text{ l/sec}$$

→ for $L/D < 5$, above equation is valid for short pipes, with error

$$L/D = 0.714$$

~+12% error max:

$$C_{shortFinal} = C_{short} \times 0.88$$

$$C_{shortFinal} = 73.420 \text{ l/sec}$$

$$\rightarrow C_{gate\ valve} = 73.420 \text{ l/sec}$$

8.) TOTAL SYSTEM CONDUCTANCE

→ Conductance of Pipeline

$$\frac{1}{C_{pipeline}} = \frac{1}{C_{baffle_adapter}} + \frac{1}{C_{baffle}} + \frac{1}{C_{plate_adapter}} + \frac{1}{C_{reducer}} + \frac{1}{C_{cross}} + \frac{1}{C_{gate_valve}}$$

$$\frac{1}{C_{pipeline}} = \frac{1}{1418.746} + \frac{1}{1421.145} + \frac{1}{879.324} + \frac{1}{118.234} + \frac{1}{36.392} + \frac{1}{73.420}$$

$$C_{pipeline} = 19.193 \text{ l/sec}$$

$$\rightarrow C_{pipeline} = 19.193 \text{ l/sec}$$

→ Effective Pumping Speed of the System

$$\frac{1}{S_e} = \frac{1}{C_{pipeline}} + \frac{1}{S_{diff}}$$

$$S_e = \frac{C_{pipeline} \times S_{diff}}{C_{pipeline} + S_{diff}}$$

$$C_{pipeline} = 19.193 \text{ l/s}$$

$$S_{diff} = 624 \text{ l/s}$$

$$S_e = 18.620 \text{ l/s}$$

$$\rightarrow S_e = 18.620 \text{ l/sec}$$